

Statistical Analysis and Optimization of Acid Dye Biosorption by Brewery Waste Biomass Using Response Surface Methodology

V. Jaikumar

Department of Chemical Engineering

SSN College of Engineering, Rajiv Gandhi Salai (OMR), Kalavakkam, Chennai 603110, India

Tel: 91-44-2747-5063 Ext 416 E-mail: jaikumarv@ssn.edu.in

V. Ramamurthi (Corresponding author) Department of Chemical Engineering, Alagappa College of Technology Anna University Chennai, Chennai 600025, INDIA Tel: 91-44-2220-3523 E-mail: vramamurthi@yahoo.co.in

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Abstract

Biosorption of Acid Yellow (AY 17) and Acid Blue (AB 25) were investigated using a biomass obtained from brewery industrial waste spent brewery grains (SBG). A 2⁴ full factorial response surface central composite design with seven replicates at the centre point and thus a total of 31 experiments were employed for experimental design and analysis of the results. The combined effect of time, pH, adsorbent dosage and dye concentration on the dye biosorption was studied and optimized using response surface methodology. The optimum contact time, pH, adsorbent dosage and dye concentration were found to be 45min, 6, 0.5g, 75 mg/L respectively for the maximum decolorization of AY 17(97.2%) and 40 min, 2, 0.4g and 75 mg/L respectively for the maximum decolorization of AB 25(97.9%). A quadratic model was obtained for dye decolourization through this design. The experimental values were in good agreement with predicted values and the model developed was highly significant, the correlation coefficient being 0.89 and 0.905 for AY 17 and AB 25 respectively. Experimental results were analyzed by Analysis of variance (ANOVA) statistical concept.

Keywords: Biosorption, Response surface methodology, Acid dyes, Spent brewery grains, Statistical analysis

1. Introduction

Dyes are intensely coloured substance used for the dyeing of various materials such as textiles, paper, leather, hair, foods, drugs, cosmetics, plastics and many more substances. They are retained on these materials by physical adsorption, salt or metal complex formation, solution mechanical retention, or by the formation of covalent chemical bonds. The colour of the dye is due to electronic transitions between various molecular orbital, the probability of these transitions determining the intensity of the colour. Textile dyes are also designed to be resistant to fading by chemicals and light. They must also be resilient to both high temperatures and enzyme degradation resulting from detergent washing. For these reasons, degradation of dyes is typically a slow process.

The effluents arising out of textile and dyeing industries are the most problematic to be treated not only for their high chemical and biological oxygen demands, suspended solids in toxic compounds but also for colour, which is the first contaminant to be recognized by human eye. Dye wastewater is usually treated by physical or chemical treatment processes for colour removal. These include chemical coagulation/flocculation, precipitation, ozonation, adsorption, oxidation, ion exchange, membrane filtration and photo degradation. These methods for colour removal from effluents have high operating costs and limited applicability (Cooper, 1993). In recent years, biological decolourization method has been considered as an alternative and eco-friendly economical method. This has led many researchers to search for the use of effective, economical and eco-friendly alternative materials such as Chitin (McKay et *al.*, 1983); Silica

(McKay, 1984); the hardwood sawdust (Asfour et *al.*, 1985); Bagasse pith (McKay et *al.*, 1987); Fly ash (Khare et *al.*, 1987); Paddy straw (Deo, 1993); Rice husk (Lee & Low, 1997); Slag (Ramakrishna & Viraraghavan, 1997); Chitosan (Juang et *al.*, 1997); Palm fruit bunch (Nasser, 1997); Bone char (Ko et *al.*, 2000). Thus research is still going on to develop alternative low cost adsorbents to activated carbon which is used mostly in industries. So in the present study spent brewery grains (SBG) which is present in abundant as waste in brewery industry is tried and tested as biosorbent.

Except a few studies in the literature for colour removal only traditional methods of experimentation were followed to study the effects of all variables which are lengthy, random processes and also require large number of experimental combinations to obtain the desired results. In addition, obtaining the optimum conditions i.e., the point at which maximum % colour removal could be achieved is almost beyond the scope. The traditional step-by-step approach, although widely used, involves a large number of independent runs and does not enable us to establish the multiple interacting parameters. This method is also time consuming, material consuming and requires large number of experimental trials to find out the effects, which are unreliable. So, specifically designed experiments to optimize the system with lesser number of experiments are the need of the hour. These limitations of the traditional method can be eliminated by optimizing all the affecting parameters collectively by statistical experimental design (Montgomery, 1991).

So, in this present study, experiments were designed by incorporating all important process variables namely time, pH, adsorbent dosage, and initial dye concentration using Statistical Design Software Minitab 14 (USA). Experimental design allows a large number of factors to be screened simultaneously to determine which of them has a significant effect on % colour removal. A polynomial regression response model shows the relationship of each factor towards the response as well as the interactions among the factors. Those factors can be optimized to give the maximum response (% colour removal) with a relatively lower number of experiments. In this context, a new approach using statistically designed experiments for finding optimum conditions for maximum % colour removal was discussed in detail. The corresponding interactions among the variables were studied and optimized using central composite design and response surface and contour plots.

2. Materials and Methods

2.1 Biosorbent and Adsorbate

The Brewery Industry waste Spent Brewery grain was obtained from Mohan breweries and distilleries Limited, Chennai, India and dried at 60°C for 12 hours. Synthetic textile dye acid yellow and acid blue was obtained from Sigma-Aldrich Chemicals Private Ltd., India and was used without further purification their chemical structures are shown in Fig.1 and Fig.2. All chemicals and reagents used for experiments were of analytical grade and supplied by Qualigens fine chemicals.

2.2 Preparation of biomass

Spent Brewery Grains, taken from Mohan breweries and distilleries Limited, Chennai, India, was suspended in 1M sulphuric acid solution (20g of SBG per 100mL of acid solution) for one hour. Then it was filtered and the acid solution was discarded. The biomass was washed with distilled water many times until it is completely free from the acid and dried at 60°C for 24 hours. The dried biomass was ground, sieved to 270 mesh size and stored for further use in the experiments. As seen from the Fig.3 the scanning electron micrograph (SEM) image shows the porous structure of the biosorbent.

2.3 Batch Experiments

Stock solution 1000mg/L of dye (AY 17 and AB 25) were prepared in double distilled water and was diluted as required according to the working concentration. The required pH was adjusted by 0.1N HCl or 0.1N NaOH. pH was measured using a pH meter (Elico, model LI 120, Hyderabad, India). Dye concentration was measured using UV–Vis Spectrophotometer (HITACHI U 2000, spectrophotometer) at a wavelength corresponding to the maximum absorbance of each dye $\lambda_{max} = 401.5$ nm for AY 17 and $\lambda_{max} = 600$ nm for AB 25. The dye solution (50 mL) at desired concentration, pH and adsorbent dosage taken in 250 ml Erlenmeyer flasks was contacted. The flasks were kept under agitation in a rotating orbital shaker at 150 rpm for desired time. Experiments were performed according to the central composite design (CCD) matrix given in Table 2. The response was expressed as % color removal calculated as

$$\% Colourremoval = \left[\frac{C_0 - C_t}{C_0}\right] \times 100$$
⁽¹⁾

2.4 Factorial experimental design

The parameters contact time, pH, adsorbent dosage and dye concentration were chosen as independent variables and the output response, removal efficiency of dye. Independent variables, experimental range and levels for AY 17 and AB 25 removal are given in Table 1 and Table 2. A 2^4 full-factorial experimental design, with seven replicates at the center point and thus a total of 31 experiments were employed in this study. The center point replicates were chosen to verify any change in the estimation procedure, as a measure of precision property. Experimental plan showing the coded value

of the variables together with dye removal efficiency are given in Table 3.The analysis focused on how the colour removal efficiency is influenced by independent variables, i.e., time (X_1) , pH(X₂), adsorbent dosage(X₃) and dye concentration(X₄).The dependent output variable is maximum removal efficiency. For statistical calculations, the variables X_i were coded as x_i according to the following relationship:

$$x_i = \left[\frac{X_i - X_0}{\delta X}\right] \tag{2}$$

The behavior of the system was explained by the following quadratic equation

$$Y = \beta_0 + \sum \beta_i x_i + \sum \beta_{ij} x_i^2 + \sum \beta_{ij} x_i x_j$$
(3)

The results of the experimental design were studied and interpreted by statistical software, MINITAB 14 (PA, USA) to estimate the response of the dependent variable.

3. Results and Discussion

3.1Response Surface Methodology (RSM)

The most important parameters, which affect the efficiency of a biosorption process are contact time, pH, adsorbent dosage and dye concentration. In order to study the combined effect of these factors, experiments were performed at different combinations of the physical parameters using statistically designed experiments.

The main effects of each parameter on dye removal are given in Fig.4 and Fig.5 for AY 17 and AB 25 respectively. From the figure, it was observed that the maximum removal was found to occur at 60 min for AY 17 and 45 min for AB 25. This indicates that higher the contact time between the dye and adsorbent, higher is the equilibrium removal efficiency. Maximum adsorption occurred at acidic pH range for both the acid dyes. This may be due to high electrostatic attraction between the positively charged surface of the SBG and anionic dyes AY 17 and AB 25. Acid dyes are also called as anionic dyes because of the negative electrical structure of the chromophore group. As the initial pH increases, the number of negatively charged sites on the biosorbent surfaces increases and the number of positively charged sites decreases. A negative surface charge does not favor the biosorption of dye anions due to electrostatic repulsion (Namasivayam and Kavitha, 2002). In general, the acidic dye uptakes are much higher in acidic solutions than those in neutral and alkaline conditions.

It was observed that the removal efficiency of both the dyes AY 17 and AB 25 increases as the adsorbent dosage increases. This may be due to the increase in the available active surface area of the adsorbent. It is observed that the removal efficiency of AY 17 decreases with the increase in dye concentration due to unavailability of surface area of the adsorbent to the increasing number of dye molecules and for AB 25 it is increasing in the studied range up to 175 mg/L with increase in initial dye concentration. Using the experimental results, the regression model equation (second order polynomial) relating the removal efficiency and process parameters was developed and is given in Equ. (4). and Equ. (5) for AY 17 and AB 25 respectively.

The regression equation for the determination of output response for AY17 is

 $\eta = (62.7143) + (2.5590X_1) + (-2.6632X_2) + (12.5382X_3) + (-5.4092X_4) + (-0.2117(X_1^2) + (-4.4617X_2^2) + (0.2883X_3^2) + (1.9609X_4^2) + (0.1823X_1X_2) + (0.5469X_1X_3) + (0.8073X_1X_4) + (-0.3906X_2X_3) + (0.5990X_2X_4) + (-0.9115X_3X_4)$ (4)

The regression equation for the determination of output response for AB 25 is

 $\eta = (96.8571) + (0.9867X_1) + (-1.8254X_2) + (-0.3079X_3) + (0.5308X_4) + (-2.1964(X_1^2) + (-0.5897X_2^2) + (0.1089X_3^2) + (0.0909X_4^2) + (-1.5768X_1X_2) + (0.5658X_1X_3) + (-0.0163 X_1X_4) + (-0.0653 X_2X_3) + (0.4310 X_2X_4) + (-0.0572 X_3X_4) (5)$

Apart from the linear effect of the parameter for the dye removal, the RSM also gives an insight into the quadratic and interaction effect of the parameters. These analyses were done by means of Fisher's '*F*'-test and Student't'-test. The student't'-test was used to determine the significance of the regression coefficients of the parameters. The *P*-values were used as a tool to check the significance of each of the interactions among the variables, which in turn may indicate the patterns of the interactions among the variables. In general, larger the magnitude of *t* and smaller the value of *P*, the more significant is the corresponding coefficient term (Montgomery, 1991). The regression coefficient, *t* and *P* values for all the linear, quadratic and interaction effects of the parameter are given in Table 4 and Table 5 for AY 17 and AB 25. It was observed that the coefficients for the linear effect of time was the least significant for AY 17 and pH, time (*P* = 0.000, 0.004, respectively) was highly significant and coefficient for the linear effect of pH and dye concentration (*P* = 0.002, 0.130) was highly significant and the coefficient of the quadratic terms of time (*P* = 0.865) was least significant for AY 17.The coefficient of the quadratic terms of time (*P* = 0.737) was least significant for AB 25.

The coefficients of the interactive effects of AY 17 among the variables did not appear to be very significant in comparison to the interactive effects of AB 25. However, the interaction effect between time and pH (P = 0.000) and time and adsorbent dosage (P = 0.131) were found to be significant for AB 25. The significance of these interaction effects between the variables would have been lost if the experiments were carried out by conventional methods.

The optimum values of the process variables for the maximum removal efficiency for both the dyes AY 17 and AB 25 are shown in Table 6. These results are in close agreement with those obtained from the response surface analysis, confirming that the RSM could be effectively used to optimize the process parameters in complex processes using the statistical design of experiments. Although few studies on the effects of parameters on adsorption have been reported in the literature, only a few attempts has been made to optimize them using statistical optimization methods. The predicted values (using the model equation) were compared with experimental result and the data are shown in Table 3.

3.2 Analysis of Variance (ANOVA)

The statistical significance of the ratio of mean square due to regression and mean square due to residual error was tested using analysis of variance (ANOVA). ANOVA is a statistical technique that subdivides the total variation in a set of data into component parts associated with specific sources of variation for the purpose of testing hypothesis on the parameters of the model (Segurola et *al.*, 1999). According to the ANOVA Table 7 and Table 8 for AY 17 and AB 25, the $F_{\text{Statistics}}$ values for all regressions were higher. The large value of F indicates that most of the variation in the response can be explained by the regression model equation. The $F_{\text{statistics}}$ value of 9.24 is greater than tabulated $F_{14, 16}$ (2.38) which indicates that the second order polynomial equation (4) is highly significant and adequate to represent the actual relationship between the response and the variables with a high value of coefficient of determination (R = 0.9433; $R^2 = 0.89$) for AY 17. The $F_{\text{statistics}}$ value of 10.9 is greater than tabulated $F_{14, 16}$ (3.14) which indicates that the second order polynomial equation (R = 0.9513; $R^2 = 0.905$) for AB 25.

The associated *P*-value is used to judge whether *F* Statistics is large enough to indicate statistical significance. A *P*-value lower than 0.05 indicates that the model is considered to be statistically significant (Kim et *al.*, 2003). The *P*-values for almost all of the regressions for both the acid dyes AY 17 and AB 25 were lower than 0.01. This means that at least one of the terms in the regression equation has a significant correlation with the response variable. The ANOVA table also shows a term for residual error, which measures the amount of variation in the response data left unexplained by the model. The form of the model chosen to explain the relationship between the factors and the response is correct.

The response surface and contour plots to estimate the removal efficiency over independent variables adsorbent dosage, pH and pH, dye concentration for the dyes are shown in Fig.6 and 7 for AY 17 and Fig.8 and 9 for AB 25 respectively. The contour plots given in figures show the relative effects of any two variables when concentration of the remaining variables is kept constant. The maximum predicted yield is indicated by the surface confined in the smallest curve of the contour diagram (Gopal et *al.*, 2002).

Figs. 10 - 13 depict the experimental and model predicted removal efficiencies. The predictive capacity of the models was also evaluated in terms of the relative deviations $(RE_{Exp} - RE_{Pred}) / RE_{Exp}$ for the model. With a few exceptions, the values of the variables showed a good agreement (within 3% error) with the experimental data shown in Table 3.

4. Conclusions

The present investigation clearly demonstrated the applicability of SBG as biosorbent for AY 17 and AB 25 dye removal from aqueous solutions. Experiments were carried out covering a wide range of operating conditions. The influence of time, pH, adsorbent dosage and initial dye concentration was critically examined. It was observed from this investigation that the percentage removal efficiency is significantly influenced by time, pH, adsorbent dosage and initial dye concentration. A 2⁴ Full factorial central composite experimental design was applied. The experimental data were analyzed using response surface methodology and the individual and combined parameter effects on colour removal efficiency were analyzed. Regression equations were developed for removal efficiency using experimental data and solved using the statistical software Minitab 14. It was observed that model predictions are in good agreement with experimental observations. Under optimal values of process parameters around 97.2% and 97.9% colour removal was achieved for AY 17 and AB 25 dye respectively using the SBG. This study clearly showed that response surface methodology was one of the suitable methods to optimize the best operating conditions to maximize the dye removal.

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References

Asfour, H.M., Fadeli, O.A., Nasser, M.M., & El-Geundi, M.S. (1985). Colour removal from textile effluents using hardwood sawdust as adsorbent. *J. Chem. Technol. Biotechnol.* 35, 21-27.

Cooper, P. (1993). Removing colour from dye house wastewaters - a critical review of technology available. J Soc Dyers Colour. 109, 97-108.

Deo, N., & Ali, M. (1993). Adsorption by a new low cost material Congo red 2. Ind. J. Environ. Protect. 13, 496-508.

Gopal, M., Pakshirajan, K., & Swaminathan, T. (2002). Heavy metal removal by biosorption using phanerochaete chrysosporium. *Appl. Biochem. Biotechnol.* 102, 227-237.

Juang, R.S., Tseng, R.K.L., Wu, F.C., & Lee, S.H. (1997). Adsorption behaviour of reactive dyes from aqueous solution on chitosan. *J. Chem. Technol.* 70, 391-399.

Khare, S.K., Panday, S.K., Srivastava, R.M., & Singh, V.N. (1987). Removal of Victoria Blue from aqueous solutions by fly ash. *J. Chem. Technol. Biotechnol.* 38, 99-104.

Kim, H.M., Kim, J.G., Cho, J.D., & Hong, J.W. (2003). Optimization and characterization of UV-curable adhesives for optical communication by response surface methodology. *Polym. Test.* 22, 899-906.

Ko, D.C.K., Porter, J.F., & McKay, G. (2000). Optimized correlations for the fixed bed adsorption of metal ions on bone char. *Chem. Eng. Sci.* 55, 5819-5829.

Lee, C.K., & Low, K.S., (1997). Quaternized rice husk as sorbent for reactive dyes. Bioresour. Technol. 61, 121-125.

McKay, G., Blair, H.S., &Gardner, J.S. (1983). Rate studies for the adsorption of dyestuffs on chitin. *J.Colloid Interface Sci.* 95,108-119.

McKay, G. (1984). Analytical solution using a pore diffusion model for a pseudo irreversible isotherm for the adsorption of basic dye on silica. *J.AIChE*. 30, 692-697.

McKay, G., Geundi, E.I., & Nasser, M.M. (1987). Equilibrium studies during the removal of dyestuff's from aqueous solutions using bagasse pith. *Water Resour.* 21, 1513-1520.

Montgomery, D.C. (1991). Design and analysis of experiments. New York: Wiley.

Namasivayam, C., & Kavitha, D. (2002). Removal of Congo Red from water by adsorption onto activated carbon prepared from coir pith, an agricultural solid waste. *Dyes and pigments*. 54, 47-58.

Nasser, M.M., (1997). Intraparticle diffusion of Basic red and basic yellow dyes on Palm fruit Bunch. *Water Sci. Technol.* 40, 133-139.

Ramakrishna, K.R. & Viraraghavan, T. (1997). Use of slag for dye removal. Waste Manage. 17, 483-488.

Segurola, J., Allen, N.S., Edge, M., & Mahon, A.M. (1999). Design of eutectic photo initiator blends for UV/visible curable acrylated printing inks and coatings. *Prog. Org. Coat.* 37, 23-37.

Nomenclature

Non	nenciature
C _o	initial concentration of dye solution (mg/L)
C_t	concentration of dye solution at the desired
	time, $t (mg/L)$
REE	xp. Removal Efficiency experimental value
REp	red. Removal Efficiency predicted value
RE	Removal Efficiency
x_i	dimensionless coded value of the variable, Xi
Xo	value of the Xi at the center point
X_{l}	time (min)
X_2	pH
X_3	adsorbent dosage(g)
X_4	dye concentration (mg/L)
δX	step change
Y	predicted response
Gree	ek letters
β_0	offset term
β_i	linear effect
β_{ii}	squared effect
β_{ij}	interaction effect
η	removal efficiency

Range and level					
-a	-1	0	+1	+α	
15	30	45	60	75	
4	6	8	10	12	
0.125	0.25	0.375	0.5	0.625	
75	100	125	150	175	
	15 4 0.125	15 30 4 6 0.125 0.25	$-\alpha$ -1 0 15 30 45 4 6 8 0.125 0.25 0.375	$-\alpha$ -1 0 $+1$ 15 30 45 60 4 6 8 10 0.125 0.25 0.375 0.5	

Table 1. Experimental range and levels of independent process variables for AY 17 removal

Table 2. Experimental range and levels of independent process variables for AB 25 removal

	Range and level					
Independent variable	-α	-1	0	+1	+α	
Time(X ₁ ,min)	15	30	45	60	75	
pH(X ₂)	2	4	6	8	10	
Adsorbent dosage(X ₃ ,g)	0.2	0.4	0.6	0.8	1.0	
Dye concentration(X ₄ ,mg/L)	75	100	125	150	175	

Table 3. Full factorial central composite design matrix for AY 17 and AB 25 removal

Observations	Time (X ₁ ,min)	рН (X ₂)	Adsorbent dosage (X ₃ ,g)	Dye concentration (X4,mg/L)	Removal Efficiency (η, %)			%)
					AY	<i>K</i> 17	AB 25	
					RE _{Exp} .	RE _{Pred} .	RE _{Exp} .	RE _{Pred} .
1	-1	-1	-1	-1	53.75	54.10	97.94	98.19
2	1	-1	-1	-1	57.50	56.14	94.55	92.93
3	-1	1	-1	-1	53.75	47.99	96.07	94.51
4	1	1	-1	-1	57.50	50.77	94.11	93.01
5	-1	-1	1	-1	80.00	80.69	93.52	92.66
6	1	-1	1	-1	82.50	84.92	96.47	96.85
7	-1	1	1	-1	78.75	73.02	98.62	98.47
8	1	1	1	-1	80.00	77.98	91.50	90.04
9	-1	-1	-1	1	44.17	42.29	98.58	98.14
10	1	-1	-1	1	46.67	47.57	97.94	98.95
11	-1	1	-1	1	45.83	38.58	98.23	99.00
12	1	1	-1	1	49.17	44.58	90.44	91.15
13	-1	-1	1	1	63.33	65.23	90.29	90.65
14	1	-1	1	1	70.83	72.69	96.23	96.85
15	-1	1	1	1	62.50	59.96	96.23	96.85
16	1	1	1	1	73.33	68.15	97.52	96.67
17	-α	0	0	0	51.00	56.75	93.13	92.93
18	α	0	0	0	64.00	66.99	89.41	90.84
19	0	-α	0	0	57.00	50.19	83.64	86.09
20	0	α	0	0	24.00	39.54	96.17	95.01
21	0	0	-α	0	30.00	38.79	97.52	96.85
22	0	0	α	0	89.00	88.94	97.52	96.85
23	0	0	0	- α	76.67	81.38	91.17	91.17
24	0	0	0	α	55.71	59.74	96.47	96.85
25	0	0	0	0	61.00	62.71	92.64	92.66
26	0	0	0	0	63.00	62.71	96.06	97.90
27	0	0	0	0	63.00	62.71	96.38	98.28
28	0	0	0	0	63.00	62.71	97.52	96.85
29	0	0	0	0	63.00	62.71	94.11	94.16
30	0	0	0	0	63.00	62.71	97.05	96.15
31	0	0	0	0	63.00	62.71	93.30	92.78

Term	Coefficient	Standard error	Т	Р
Constant	62.7143	2.484	25.247	0.000
X ₁	2.5590	1.342	1.908	0.075
X ₂	-2.6632	1.342	-1.985	0.065
X ₃	12.5382	1.342	9.346	0.000
X_4	-5.4092	1.342	-4.032	0.001
X ₁ X ₁	-0.2117	1.229	-0.172	0.865
X ₂ X ₂	-4.4617	1.229	-3.630	0.002
X ₃ X ₃	0.2883	1.229	0.235	0.817
X ₄ X ₄	1.9609	1.229	1.596	0.130
X ₁ X ₂	0.1823	1.643	0.111	0.913
X ₁ X ₃	0.5469	1.643	0.333	0.744
X_1X_4	0.8073	1.643	0.491	0.630
X ₂ X ₃	-0.3906	1.643	-0.238	0.815
X ₂ X ₄	0.5990	1.643	0.365	0.720
X ₃ X ₄	-0.9115	1.643	-0.555	0.587

Table 4. Estimated Regression Coefficients and corresponding T- and P- values for AY 17

Term	Coefficient	Standard error	Т	Р
Constant	96.8571	0.5380	180.027	0.000
\mathbf{X}_{1}	0.9867	0.2906	3.396	0.004
X ₂	-1.8254	0.2906	-6.282	0.000
X ₃	-0.3079	0.2906	-1.060	0.305
X_4	0.5308	0.2906	1.827	0.086
X_1X_1	-2.1964	0.2662	-8.251	0.000
X ₂ X ₂	-0.5897	0.2662	-2.215	0.042
X ₃ X ₃	0.1089	0.2662	0.409	0.688
X_4X_4	0.0909 0.2662		0.342	0.737
X_1X_2	X_1X_2 -1.5768 0.3559		-4.431	0.000
X ₁ X ₃	0.5658	0.3559	1.590	0.131
X_1X_4	-0.0163	0.3559	-0.046	0.964
X ₂ X ₃	-0.0653	0.3559	-0.184	0.857
X_2X_4	0.4310	0.3559	1.211	0.243
X ₃ X ₄	-0.0572	0.3559	-0.161	0.874

Table 5. Estimated Regression Coefficients and corresponding T- and P- values for AB 25

Table 6. Optimum values of the process parameter for maximum efficiency for AY 17 and AB 25

Parameter	Optimum Values		
	AY 17	AB 25	
η (Removal Efficiency, %)	97.2	97.9	
X1 (Time, min)	45	45.00	
X2 (pH)	6	2.00	
X3 (Adsorbent Dosage, g)	0.5	0.4	
X4 (Dye Concentration, mg/L)	75	75	

Table 7. ANOVA of removal efficiency	v for AY 17: Effect of time, p	H, adsorbent dosage and Dye concentration

Source	Degree of freedom	Sum of Squares	Mean of Squares	F _{statistics}	Р
Model	14	5588.78	399.2	9.24	0.000
Linear	4	4802.57	1200.64	27.8	0.000
Square	4	748.99	187.25	4.34	0.015
Interaction	6	37.22	6.20	0.14	0.988
Residual Error	16	691.08	43.19	-	-
Lack of fit	10	687.65	68.77	120.34	0.000
Pure Error	6	3.43	0.57	-	-
Total	30	6279.86	-	-	-

Table 8. ANOVA of removal efficiency for AB 25: Effect of time, pH, adsorbent dosage and Dye concentration

Source	Degree of freedom	Sum of Squares	Mean of Squares	F _{statistics}	Р
Model	14	309.256	22.0897	10.90	0.000
Linear	4	112.373	28.0933	13.86	0.000
Square	4	148.881	37.2203	18.37	0.000
Interaction	6	48.002	8.0003	3.95	0.013
Residual Error	16	32.420	2.0262	-	-
Lack of fit	10	29.992	2.9992	7.41	0.012
Pure Error	6	2.428	0.4047	-	-
Total	30	341.676	-	-	-

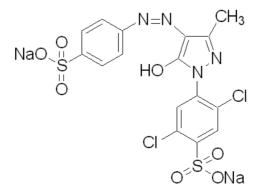


Figure 1. The chemical structure of AY 17 dye

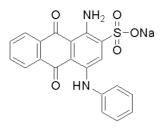


Figure 2. The chemical structure of AB 25 dye

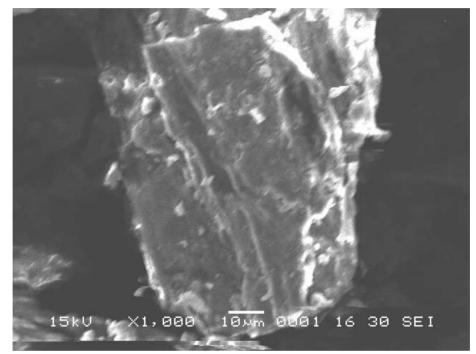


Figure 3. SEM image of the biomass SBG

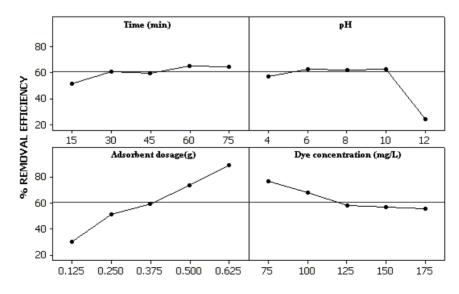


Figure 4. Main effects plot of parameters for AY 17 removal

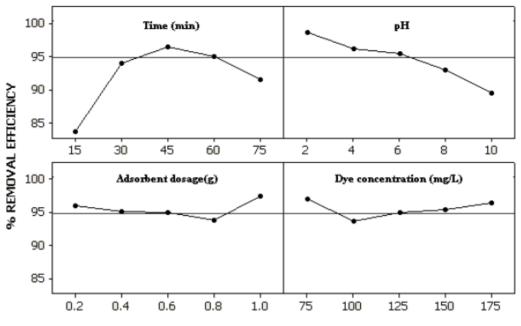


Figure 5. Main effects plot of parameters for AB 25 removal

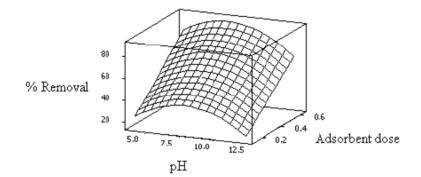


Figure 6. Response surface plot of AY 17 dye removal (%) showing interactive effect of adsorbent dose and pH

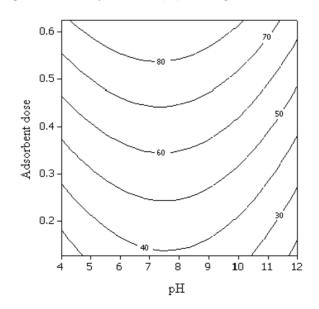


Figure 7. Response contour plot of AY 17 dye removal (%) showing interactive effect of adsorbent dose and pH.

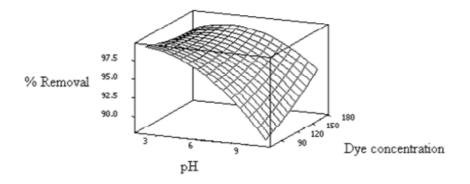


Figure 8. Response surface plot of AB 25 dye removal (%) showing interactive effect of pH and dye concentration

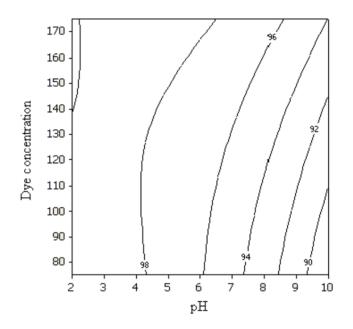


Figure 9. Response contour plot of AB 25 dye removal (%) showing interactive effect of pH and dye concentration

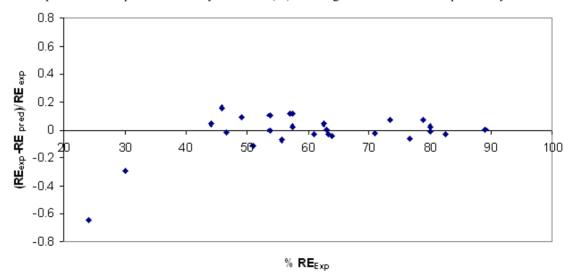


Figure 10. Comparison of experimental and predicted removal efficiency for AY 17

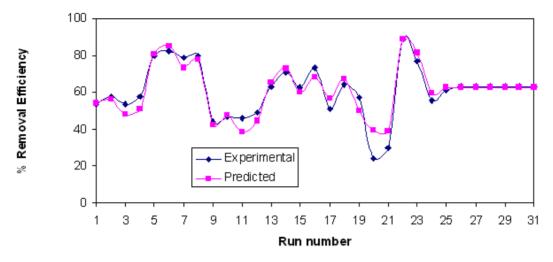


Figure 11. Relative deviation between experimental and predicted removal efficiency for AY 17

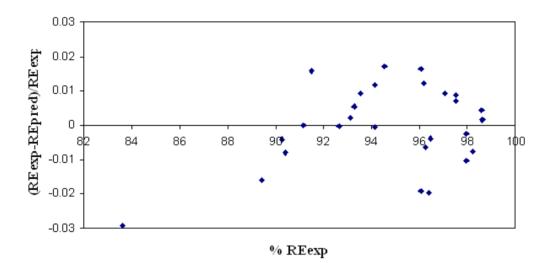


Figure 12. Comparison of experimental and predicted removal efficiency for AB 25

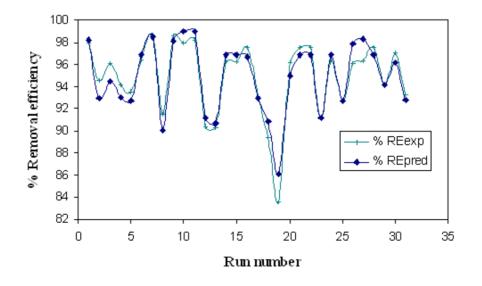


Figure 13. Relative deviation between experimental and predicted removal efficiency for AB 25