Electrocatalytic Production of Hydrogen Using Iron Sulfur Cluster

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Abstract

In response to the energy crisis, rising fossil fuel costs and global climate warming, this study focuses on the electrocatalytic reduction of proton into hydrogen using an iron sulfur cluster in the presence of pentafluorothiophenol. The direct reduction of pentafluorothiophenol at vitreous carbon electrode occurs at E_p -1.3 V *vs* Ag/AgCl in Tetrabutylammonium tetrafluoroborate [Bu₄N][BF₄]-DMF solution. Interestingly, in the presence of Iron Sulfur Cluster [Fe₄S₄(SPh)₄][Bu₄N]₂, the reduction potential shifts significantly to -0.98 V *vs* Ag/AgCl. Based on gas chromatography analysis, the formation of H₂ has been confirmed with a current efficiency of *ca*. 63% after two hours, while the chemical yield at the carbon electrode was about 46%. On the other hand, no H₂ gas was detected without catalyst. Importantly, the increment of the concentration of acid (up to 18 equivalents) led to a positive shifting in the reduction potential until a value of 0.18 V. These results reflect the exquisite electrocatalytic efficiency of the protein-like iron sulfur cluster in Hydrogen Evolution Reaction (HER).

Keywords: electrocatalysis, hydrogen, iron sulfur cluster

1. Introduction

The exquisite target of using hydrogen as sustainable energy has attracted significant attention because of many advantages including its innocent impact on the environment with energy conversion free of CO_2 emission. However, the ultimate problem resulting from its production – mostly from fossil fuels such as coal and oil-remains in the release of CO_2 which endanger the environment and global health (Aulice, 2004 & Maria, 2007) Therefore, researchers are interested in developing many other methods for hydrogen production including water splitting and proton reduction (Artero, 2014; Bhugun, 1996; Kumar, 2010; Bak, 2002 & Kelly, 2008).

Transition metal complexes are of great interest for electrocatalytic reduction of proton into hydrogen at low potential (Perutz, 2012; Kellett, 1985; Koper, 2013; David, 2015 & Han, 2014). Alenezi (2017) has studied the electrochemical catalysis of proton reduction into hydrogen using mesotetrakis-(pentafluorophenyl)porphyrin iron(III) chloride in the presence o triethylamine hydrochloride f Et₃NHCl as source of proton. The reduction potential E_p was marked with a significant shift from -1.6 V to -1.3 V *vs* Ag/AgCl in the presence of the catalyst. A current efficiency of *ca*. 58% after 3.8 h was recorded, with a yield of 8 µmoles and a turnover number of 8 while the chemical yield was about 80%. On the other hand, {Fe₄S₄}-clusters have been known for over 40 years. However, the studies of their electrocatalytic properties have been extremely limited. These entities, commonly known as iron sulfur clusters, play important roles in biological systems; they are involved in electron transfer as well as catalytic, structural, and sensory roles (Pickett, 2003 & Goh, 1996). In this study, we focus on the electrochemical catalysis of proton reduction into hydrogen using the synthetic iron sulfur complex [Fe₄S₄(SPh)₄]²⁻ at the vitreous carbon electrode in [Bu₄N][BF₄]-DMF solution.

2. Methed

Pentafluorothiophenol was purchased from Aldrich and used as received. N,N/-dimethylformamide (DMF) was purified by distillation over calcium hydride. The iron sulfur cluster $[Fe_4S_4(SPh)_4][Bu_4N]_2$ was prepared according to the literature method (Pamphilis, 1974). Electrochemical experiments were conducted to evaluate the electrocatalytic production of hydrogen by iron sulfur clusters following a reported procedure (Alenezi, 2017).

Cyclic voltammetry experiments were carried out using an Autolab PGSTAT 30 potentiostat. A conventional three-electrode arrangement was employed, consisting of a vitreous carbon working electrode (0.07 cm^2) , a platinum wire as the auxiliary electrode (2 cm^2) , and Ag⁺/AgCl as a reference electrode.

The electrolysis cell, containing 14 ml of a solution of electrolyte [NBu₄][BF₄], 0.2 M in DMF, was degassed with argon

gas. 5 ml of this solution was placed in the working electrode compartment. About 9-10 ml of the gas phase took place at the working electrode part. 1 mM of the catalyst $[Fe_4S_4(SPh)_4]^{2-}$ was added and stirred under argon in the electrochemical cell.

The electrolysis was carried out at -0.85 V vs Ag⁺/AgCl and the current were recorded during the course of electrolysis vs time; the electrolysis was stopped when the current decayed after two hours. Gas chromatography was carried out using a Perkin-Elmer Clarius 500 instrument, fitted with a 5Å molecular sieve column (800/100 mesh, 6' x 1/8") and thermal conductivity detector. The operating conditions were: 80 °C oven temperature, 0.5 ml injected volume, and 10 min retention time. The external standard calibration was performed on the same day

3. Results

3.1 Cyclic Voltammetry of 1 mM $[Fe_4S_4(SPh)_4]^{2-}$ in DMF-0.2M $[Bu_4N][BF_4]$

The cyclic voltammetry of $[Fe_4S_4(SPh)_4]^2$ - in non-aqueous electrolytes $[Bu_4N][BF_4]$ -DMF was studied. In this solvent, there is a diffusion-controlled primary reduction step, corresponding to the $[Fe_4S_4(SPh)_4]^{2-/3-}$ couple at -0.98 V vs Ag/AgCl. In addition, a second partly reversible reduction wave was observed at a more negative potential -1.72 V vs Ag/AgCl (figuer 1). Herein, the electrochemical study was carried out at the first wave reduction of $[Fe_4S_4(SPh)_4]^{2-}$.



Figure 1. Cyclic voltammetry of 1 mM $[Fe_4S_4(SPh)_4]^{2-}$ in DMF – 0.2M $[Bu_4N][BF_4]$; scan rate 100mVs⁻¹, vitreous carbon electrode under Ar at 25°C

Figure 2 shows a set of voltammograms recorded at various scan rates for $[Fe_4S_4(SPh)_4]^{2-1}$ mM in DMF– $[Bu_4N][BF_4]$. The primary reduction process is a diffusion-controlled reversible one-electron step. Thus: (i) the plot of the peak current ${}^{1}i_{p}^{red}$ vs v^{1/2} is linear, with an intercept close to zero (Figure 3); (ii) the peak potential separation of the first wave, $\Delta E_p = E_p^{ox} - E_p^{red} = \frac{59}{n}$ mV. $\Delta E = 70$ mV (theoretical separation for a one-electron process is *ca* 59 mV at 298K). The diffusion coefficient for 0.5 mM $[Fe_4S_4(SPh)_4]^{2-}$ is estimated to be 1.42 x 10⁻⁵ cm² s⁻¹, according to Randles – Sevcik Equation:

$$I_{p} = -(2.69 \times 10^{5}) n^{3/2} C_0 D^{1/2} v^{1/2}$$
. (Mabbott, 1983) 1.1

The C_0 is the bulk concentration in mol/cm³, D is the diffusion coefficient in cm² s⁻¹, *v* is the potential scan rate in V s⁻¹, and I is the current density. The electrocatalysis was carried out at the potential of the first reduction wave of $[Fe_4S_4(SPh)_4]^2$, in both presence and absence of pentafluorothiophenol.



Figure 2. Cyclic voltammograms of 1mM [Fe₄S₄(SPh)₄]² at carbon electrode, at different scan-rates in DMF containing 0.1M [NBu₄][BF₄]



Figure 3. Plot of i_p^{red} for the $[Fe_4S_4(SPh)_4]^{2-/3}$ couple versus the square-root of the scan-rate 3.2 Cyclic Voltammetry of $[Fe_4S_4(SPh)_4]^{2-}$ in the Presence of Pentafluorothiophenol

We examined the cyclic voltammetry of $[Fe_4S_4(SPh)_4]^{2-}$ in the presence of pentafluorothiophenol as a source of proton (Figure 4). The primary reduction wave for $[Fe_4S_4(SPh)_4]^{2-}$ increase in height and became irreversible while increasing the concentration of pentafluorothiophenol, which is consistent with the electrocatalysis of proton reduction by the $[Fe_4S_4(SPh)_4]^{2-}$ complex. In addition the potential shift is proportional to the concentration of pentafluorothiophenol; at a concentration as high as 18 mM, the potential shifts in about 180 mV. At high concentrations of pentafluorothiophenyl, we observe a plateau (Figure 5) for the peak current and a precipitate is formed.



Figure 4. The cyclic voltammetry of $[Fe_4S_4(SPh)_4]^2$ at low concentrations of pentafluorothiophenol



Figure 5. The cyclic voltammetry of $[Fe_4S_4(SPh)_4]^2$ in the presence of high concentrations of pentafluorothiophenol Figure 6 shows the variation of the peak current as a function of the concentration of pentafluorothiophenol. The current was enhanced with an increment of pentafluorothiophenol concentration, up to about 12 eq [12 mM]. After this concentration, the electrocatalysis became independent of the acid concentration.



Figure 6. the peak current as a function of the concentration of pentafluorothiophenol



Figure 7. Effect of the acid concentration on i_{cat} /_{i0} ratio at a vitreous carbon electrode

The kinetics of the electrocatalysis of proton reduction by $[Fe_4S_4(SPh)_4]^2$ were also investigated. The peak catalytic current was normalized by dividing the peak current for the catalyzed process by that of the uncatalyzed process (i_{cat} / i_o)

at 100 mVs⁻¹; this simplify the subsequent analysis by eliminating the surface area, along with the catalyst concentration and its diffusion coefficient (DuBois, 2013). Figure 7 shows a plot of the i_{cat}^{1}/i_{o} , where i_{cat}^{1} is the peak current measured at 100 mVs⁻¹ for the primary catalysis in the presence of different concentrations and i_{o} is the peak current measured for the first one-electron reduction step at the same scan rate in the absence of the proton source. It is important to mention that at the vitreous carbon electrode, the values of i_{cat}/i_{0} become independent of the acid concentration at *ca* 12 M in DMF- containing 0.1M [NBu₄] [BF₄].

Following the approach of Dubois and others (*DuBois, 2013*), the rate constant k_{obs}^{C} at the carbon electrode can be estimated from the i_{cat} / i_0 data using the relationship shown in Equation 1.1, where *F*, *R*, and *T* are the Faraday constant, the gas constant, and the temperature respectively, and n is the number of electrons involved in the turnover with i_{obs} , measured at the potential where the current approaches a plateau at -0.98 V vs Ag/AgCl. The value of k _{obs} is 18.9 s⁻¹.

$$K_{obs} = 0.1992 \ (Fv/RTn^2) \ (i_{cat}/i_0)^2$$
 1.2

3.3 Preparative Electrocatalysis

Preparative bulk electrolysis reduction of protons in the presence of 0.5 mM $[Fe_4S_4(SPh)_4]^{2-}$ (2.5 µmoles) was carried out in a closed system at -0.85 V vs Ag/AgCl (0.2 mM-[NBu₄][BF₄]-CH₃CN; 296 K) using 18 mM (18 equivalents, H⁺ 22.5 µmoles) of pentafluorothiophenol as a source of protons. The decay in current was monitored during the course of the experiment, while the working electrode compartment was stirred at a constant rate during electrocatalysis. Figure 8 shows the relationship between the current and time.



Figure 8. The relationship between the current and time /h

During proton reduction, the initial current rapidly decayed to a proportion of about 10% of the initial current before falling off toward the end of electrolysis; the gas phase of the cell was analyzed by gas chromatography. The gas chromatography (GC-TCD) test confirmed the formation of H₂ with a current efficiency of ca 63% after two hours, which needed to be 3.2 C, while the yield of H₂ was 10.4 μ moles. No H₂ was formed at -0.85 V vs Ag/AgCl in the presence of 18 mM of pentafluorothiophenol and absence of [Fe₄S₄(SPh)₄]² (control experiment) (Table 1).

Cable 1. Elecatrocatalysis results	ilts of proton redu	ction in the presence and	absence of [Fe ₄ S ₄ (SPh) ₄] ²
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	CPE Potential (Ag/AgCl)	Number of moles of catalyst µmole	Time of experiment/h	Charge coulomb/C	Current efficiency* H ₂	Chemical yield %	T.N H ₂
In the presence of $[Fe, S, (SPh), 1^2]$	-0.85	2.5	2	3.2	63	46.3	4.1
Control experiment	-0.85	0	2	0.12	0	0	0

In a separate experiment under the same conditions, the yield of H_2 was studied by gas chromatography as a function of electrolysis time and the charge passed versus current efficiency. Clearly, the yield of H_2 increased steadily in the first phase of the electrolysis and dropped off in the latter stages as the acid was consumed. The chemical yield of dihydrogen at the end of electrolysis, based upon the total acid available, was 43%; the electrochemical results are shown in Table 2. At the end of the electrolysis, a charge of 3.6 coulombs was passed and 5 µmoles of dihydrogen was detected in the headspace of the catholyte by thermal conductivity gas. All results show in figure 9.



Figure 9. a) The yield of dihydrogen as a function of time / h, b) The current efficiency *versus* time / h. c). The charge passed *versus* time / h

Table 2.	Current efficiency and	turnover numbers for	r electrocatalyti	ic reduction of p	protons by	$[Fe_4S_4(SPh)_4]^2$	
	2		2		2	E · · · · · / · J	

1.5	2
2.2	
3.2	3.4
53	54
40	43
3.5	3.96
3.5	3.96
3.32	3.52
-	5.2 53 40 3.5 3.5 3.32

3.4 Stability of Catalyst $[Fe_4S_4(SPh)_4]^{2-1}$

The figure 10 show that the stability of $[Fe_4S_4(SPh)_4]^{2-}$ in DMF – 0.2M $[Bu_4N][BF_4]$ was studied in presence of 18 mM of pentafluorothiophenol by comparing the difference in cyclic voltammetry before the addition of acid and after the electrocatalysis course (*fig. 10*). The peak current of the first reduction wave of $[Fe_4S_4(SPh)_4]^{2-}$ before the addition of the acid source was 2.36 μ A, while after the electrocatalysis course it was 1.742 μ A. This confirms that 73% of $[Fe_4S_4(SPh)_4]^{2-}$ was recovered after two hours.



Figure 10. Cyclic voltammetry of $[Fe_4S_4(SPh)_4]^{2-}$ before addition of pentafluorothiophenol and after electrolysis course

4. Conclusion

We have shown here that $[Fe_4S_4(SPh)_4]^{2-}$ is a powerful catalyst for the reduction of proton into hydrogen at the carbon electrode in DMF- $[Bu_4N][BF_4]$ at 23 ⁰C. The cyclic voltammogram of $[Fe_4S_4(SPh)_4]^{2-}$ displayed two successive reversible reduction peaks; at -0.98V and -1.72V *vs* Ag/AgCl. The HER occurs at $E_p = -0.98V$ which is a significant shift comparing to $E_p = -1.3$ V; the reduction potential of pentafluorothiophenol without catalyst. The addition of high concentration of pentafluorothiophenol led to a positive shifting in the potential; while adding 18 equivalents, the potential shifts about 450 mV. The current efficiency to produce dihydrogen was about 63%, while the chemical yield was 46% and the turnover number was 4 after *ca*. 2 hours.

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